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L2: Entry 1 of 1

File: DWPI

Nov 30, 1994

DERWENT-ACC-NO: 1995-205005

DERWENT-WEEK: 199527

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TITLE: Highly dispersed colloidal sulphur in high yield - by oxidn. of methane contg. hydrogen sulphide in pseudo-liq. catalyst layer

INVENTOR: ISMAGILOV, F R; KHAIRULIN, S R ; MOISEEV, S A

PATENT-ASSIGNEE:

ASSIGNEE

CODE

BASHKIR GROZNEFTEKHIM SCI PRODN ASSOC

BASHR

PRIORITY-DATA: 1991SU-4954166 (June 5, 1991)

PATENT-FAMILY:

PUB-NO

PUB-DATE

LANGUAGE

PAGES

MAIN-IPC

RU 2023655 C1

November 30, 1994

004

C01B017/04

APPLICATION-DATA:

PUB-NO

APPL-DATE

APPL-NO

DESCRIPTOR

RU 2023655C1

June 5, 1991

1991SU-4954166

INT-CL (IPC): B01D 53/36; C01B 17/04

ABSTRACTED-PUB-NO: RU 2023655C

BASIC-ABSTRACT:

Hydrocarbon gas contg. sulphur is oxidised with air at 250-300deg.C and a ratio of H₂S:O₂ of 0.50-0.51 in presence of a catalyst contg. oxides of chromium, magnesium and vanadium in the ratio 16-18 : 4.0-5.2 : 3.5-4.2, with aluminium oxide to 100 wt.%, in a pseudo-liq. layer. The product is treated with water at 60-85deg.C.

USE - The sulphur is used in production of herbicides for fruit and vegetables, and in the plastics industry.

ADVANTAGE - The method uses waste sulphur-contg. gas to give highly dispersed sulphur of particle size 0.5-5 mkm., in a yield of 85% compared to the previous 65%.

CHOSEN-DRAWING: Dwg.0/0

TITLE-TERMS: HIGH DISPERSE COLLOID SULPHUR HIGH YIELD OXIDATION METHANE CONTAIN HYDROGEN SULPHIDE PSEUDO LIQUID CATALYST LAYER

DERWENT-CLASS: A60 C03 E36

CPI-CODES: A08-C04; C05-C06; C12-M07; E31-F02; N01-B; N03-C01; N03-D01;

CHEMICAL-CODES:

Chemical Indexing M2 *01*

WEST**End of Result Set**

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L1: Entry 1 of 1

File: DWPI

Sep 23, 1994

DERWENT-ACC-NO: 1994-304872
DERWENT-WEEK: 199908
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TITLE: A procedure for the direct oxidn. of hydrogen sulphide to sulphur - in hydrogen sulphide contg. gases using a metallic catalyst supported on activated charcoal.

INVENTOR: ANGLEROT, D; DEMARAIS, G ; MAILLES, P

PATENT-ASSIGNEE:

ASSIGNEE

CODE

ELF AQUITAINE PRODN

ERAP

ELF EXPLORATION PRODN

ERAP

ELF AQUITAINE PRODN SA

ERAP

ELF AQUITAINE

ERAP

PRIORITY-DATA: 1993FR-0002996 (March 16, 1993)

PATENT-FAMILY:

PUB-NO	PUB-DATE	LANGUAGE	PAGES	MAIN-IPC
FR 2702675 A1	September 23, 1994		018	B01D053/36
NO 304501 B1	January 4, 1999		000	B01D053/52
WO 9421358 A1	September 29, 1994	F	016	B01D053/36
NO 9404356 A	January 9, 1995		000	B01D053/52
EP 640004 A1	March 1, 1995	F	000	B01D053/36
JP 07509436 W	October 19, 1995		009	C01B017/04
CN 1105174 A	July 12, 1995		000	B01D053/52
EP 640004 B1	January 14, 1998	F	009	B01D053/52
DE 69407897 E	February 19, 1998		000	B01D053/52
ES 2114185 T3	May 16, 1998		000	B01D053/52
RU 2107024 C1	March 20, 1998		000	C01B017/04

DESIGNATED-STATES: CA CN JP KZ NO RU UA US UZ AT BE CH DE DK ES FR GB GR IE IT LU MC NL
PT SE AT BE CH DE DK ES FR GB GR IE IT LI LU MC NL PT SE AT BE CH DE DK ES FR GB GR IE
IT LI LU MC NL PT SE

CITED-DOCUMENTS:DE 1809329; DE 2652099 ; EP 506160 ; FR 1603452 ; US 3790659 ; US
4054642

APPLICATION-DATA:

PUB-NO	APPL-DATE	APPL-NO	DESCRIPTOR
FR 2702675A1	March 16, 1993	1993FR-0002996	
NO 304501B1	March 16, 1994	1994WO-FR00283	
NO 304501B1	November 15, 1994	1994NO-0004356	
NO 304501B1		NO 9404356	Previous Publ.
WO 9421358A1	March 16, 1994	1994WO-FR00283	
NO 9404356A	March 16, 1994	1994WO-FR00283	
NO 9404356A	November 15, 1994	1994NO-0004356	
EP 640004A1	March 16, 1994	1994EP-0909970	
EP 640004A1	March 16, 1994	1994WO-FR00283	
EP 640004A1		WO 9421358	Based on
JP 07509436W	March 16, 1994	1994JP-0520711	
JP 07509436W	March 16, 1994	1994WO-FR00283	
JP 07509436W		WO 9421358	Based on
CN 1105174A	March 16, 1994	1994CN-0190206	
EP 640004B1	March 16, 1994	1994EP-0909970	
EP 640004B1	March 16, 1994	1994WO-FR00283	
EP 640004B1		WO 9421358	Based on
DE 69407897E	March 16, 1994	1994DE-0607897	
DE 69407897E	March 16, 1994	1994EP-0909970	
DE 69407897E	March 16, 1994	1994WO-FR00283	
DE 69407897E		EP 640004	Based on
DE 69407897E		WO 9421358	Based on
ES 2114185T3	March 16, 1994	1994EP-0909970	
ES 2114185T3		EP 640004	Based on
RU 2107024C1	March 16, 1994	1994RU-0046133	
RU 2107024C1	March 16, 1994	1994WO-FR00283	

INT-CL (IPC): B01 D 53/36; B01 D 53/52; B01 D 53/75; B01 D 53/86; B01 D 161:00; B01 J 21/00; B01 J 21/18; B01 J 23/00; B01 J 23/16; B01 J 23/22; B01 J 27/047; C01 B 17/04

ABSTRACTED-PUB-NO: EP 640004B
BASIC-ABSTRACT:

A process for the direct oxidn. of H₂S contg. gases to S, by a catalytic route is claimed. The gas is mixed with a gas contg. free O₂ in proportions such that the molar ratio O₂:H₂S is 0.5-3 (more pref. 0.5-1.5) and contacted with an oxidn. catalyst at a temp. less than 200deg.C.

The catalyst comprises an activated charcoal support in which a catalytic phase is incorporated consisting of oxides, salts or sulphides of one or several transition metals chosen from V, Mo, W, Ni and Co the amt. of activate phase (as metal) is 0.1-15% of the wt. of the calcined catalyst.

Also claimed is the catalyst used in the process.

USE - Sources of gases suitable for treatment are natural gas, gases from gasification of charcoal or heavy oils, gases contg. S cpds. such as SO₂, mercaptans, COS, CS₂ etc. convertible to H₂S by H₂ or water vapour and gases from de-sulphurisation plant contg. H₂S and SO₂.

ADVANTAGE - The invention ensures a high conversion of H₂S and high selectivity in S, it is partic. useful as a final treatment step before incineration and release to the environment.

ABSTRACTED-PUB-NO:

FR 2702675A
EQUIVALENT-ABSTRACTS:

A process for the direct oxidn. of H₂S contg. gases to S, by a catalytic route is

claimed. The gas is mixed with a gas contg. free O₂ in proportions such that the molar ratio O₂:H₂S is 0.5-3 (more pref. 0.5-1.5) and contacted with an oxidn. catalyst at a temp. less than 200 deg. C.

The catalyst comprises an activated charcoal support in which a catalytic phase is incorporated consisting of oxides, salts or sulphides of one or several transition metals chosen from V, Mo, W, Ni and Co the amt. of activate phase (as metal) is 0.1-15% of the wt. of the calcined catalyst.

Also claimed is the catalyst used in the process.

USE - Sources of gases suitable for treatment are natural gas, gases from gasification of charcoal or heavy oils, gases contg. S cpds. such as SO₂, mercaptans, COS, CS₂ etc. convertible to H₂S by H₂ or water vapour and gases from de-sulphurisation plant contg. H₂S and SO₂.

ADVANTAGE - The invention ensures a high conversion of H₂S and high selectivity in S, it is partic. useful as a final treatment step before incineration and release to the environment.

CHOSEN-DRAWING: Dwg.0/0 Dwg.0/0

TITLE-TE RMS: PROCEDURE DIRECT OXIDATION HYDROGEN SULPHIDE SULPHUR HYDROGEN SULPHIDE
CONTAIN GAS METALLIC CATALYST SUPPORT ACTIVATE CHARCOAL

DERWENT-CLASS: E36 H04 J04

CPI-CODES: E11-Q02; E31-F01B; H04-A01; H04-F02A; J04-E01; J04-E04; N02-B01; N02-C01;
N03-C; N03-C02;

CHEMICAL-CODES:

Chemical Indexing M3 *01*

Fragmentation Code

C116 C810 M411 M720 M903 M904 M910 N209 N263 N411

N441 N512 N513 Q417 Q436 Q439

Specfic Compounds

01725P

Registry Numbers

1725P

Chemical Indexing M3 *02*

Fragmentation Code

A423 A427 A428 A542 A674 C810 M411 M730 M903 Q421

Chemical Indexing M3 *03*

Fragmentation Code

C101 C116 C540 C730 C800 C801 C802 C804 C805 C806

M411 M750 M903 M904 M910 N163 N411 N441 N512 N513

Q417 Q436 Q439

Specfic Compounds

01785X

Registry Numbers

1785U

UNLINKED-DERWENT-REGISTRY-NUMBERS: 1669S; 1725P; 1779U; 1785S; 1785U

SECONDARY-ACC-NO:

CPI Secondary Accession Numbers: C1994-138959